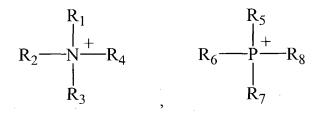
## THAT WHICH IS CLAIMED:

- 1. A catalyst system comprising an ionic liquid dispersed on a support having an average pore diameter greater than about 225 Å.
- 2. A catalyst system in accordance with claim 1 wherein said support has a surface area less than about 700 m<sup>2</sup>/gram.
- 3. A catalyst system in accordance with claim 1 wherein said support is non-crystalline.
- 4. A catalyst system in accordance with claim 1 wherein said support is non-crystalline and has a surface area less than about 700 m<sup>2</sup>/gram.
- 5. A catalyst system in accordance with claim 1 wherein said support is silica.
- 6. A catalyst system in accordance with claim 1 wherein said ionic liquid comprises a cation and an anion; wherein said cation is selected from the group consisting of ions defined by the formulas:



$$R_{10}$$
 $R_{10}$ 
 $R_{11}$ 
 $R_{12}$ 

$$R_{18}$$
 $R_{19}$ 
 $R_{15}$ 
 $R_{17}$ 
 $R_{16}$ 

and combinations of any two or more thereof, wherein:

R<sub>1</sub>, R<sub>2</sub>, R<sub>3</sub>, R<sub>5</sub>, R<sub>6</sub>, and R<sub>7</sub> are selected from saturated and unsaturated hydrocarbons containing from 1 to 7 carbon atoms per molecule;

R<sub>4</sub>, R<sub>8</sub>, R<sub>9</sub>, R<sub>10</sub>, R<sub>11</sub>, R<sub>12</sub>, R<sub>13</sub>, R<sub>14</sub>, R<sub>15</sub>, R<sub>16</sub>, R<sub>17</sub>, R<sub>18</sub>, and R<sub>19</sub> are selected from saturated and unsaturated hydrocarbons containing from 1 to 7 carbon atoms per molecule, and hydrogen; and

wherein said anion is selected from the group consisting of halides of: Group IIIA metals, copper, zinc, iron and phosphorus.

7. A catalyst system in accordance with claim 6 wherein said anion is selected from the group consisting of AlCl<sub>4</sub>, Al<sub>2</sub>Cl<sub>7</sub>, Al<sub>3</sub>Cl<sub>10</sub>, GaCl<sub>4</sub>, Ga<sub>2</sub>Cl<sub>7</sub>, Ga<sub>3</sub>Cl<sub>10</sub>, CuCl<sub>2</sub>, Cu<sub>2</sub>Cl<sub>3</sub>, Cu<sub>3</sub>Cl<sub>4</sub>, ZnCl<sub>3</sub>, FeCl<sub>3</sub>, FeCl<sub>4</sub>, Fe<sub>3</sub>Cl<sub>7</sub>, PF<sub>6</sub>, and BF<sub>4</sub>.

- 8. A catalyst system in accordance with claim 6 wherein said ionic liquid has the formula R<sub>1</sub>R<sub>2</sub>R<sub>3</sub>NH<sup>+</sup>Al<sub>2</sub>Cl<sub>7</sub>.
- 9. A catalyst system in accordance with claim 6 wherein said ionic liquid has the formula (CH<sub>3</sub>)<sub>3</sub>NH<sup>+</sup>Al<sub>2</sub>Cl<sub>7</sub>.
- 10. A catalyst system in accordance with claim 1 wherein a Group VIII metal compound is dispersed in said ionic liquid.
- 11. A catalyst system in accordance with claim 10 wherein said Group VIII metal compound comprises a platinum compound.
  - 12. A process comprising:
- a) contacting, under conversion conditions, a hydrocarbon feed stream comprising a  $C_5$  paraffin and an initiator with a catalyst system comprising an ionic liquid dispersed on a support; and
- b) withdrawing a product stream comprising a C<sub>4</sub> paraffin and at least one C<sub>6</sub> paraffin.
- 13. A process in accordance with claim 12 wherein said support has an average pore diameter greater than about 225 Å.
- 14. A process in accordance with claim 12 wherein said support has a surface area less than about 700 m²/gram.
- 15. A process in accordance with claim 12 wherein said support is non-crystalline.

- 16. A process in accordance with claim 12 wherein said support is non-crystalline, has an average pore diameter greater than about 225 Å, and has a surface area less than about  $700 \text{ m}^2/\text{gram}$ .
- 17. A process in accordance with claim 12 wherein said support is silica.
- 18. A process in accordance with claim 12 wherein said ionic liquid comprises a cation and an anion; wherein said cation is selected from the group consisting of ions defined by the formulas:

$$R_{1}$$
 $R_{1}$ 
 $R_{2}$ 
 $R_{1}$ 
 $R_{2}$ 
 $R_{3}$ 
 $R_{4}$ 
 $R_{1}$ 
 $R_{1}$ 

and combinations of any two or more thereof, wherein:

 $R_{16}$ 

 $R_{17}$ 

R<sub>1</sub>, R<sub>2</sub>, R<sub>3</sub>, R<sub>5</sub>, R<sub>6</sub>, and R<sub>7</sub> are selected from saturated and unsaturated hydrocarbons containing from 1 to 7 carbon atoms per molecule;

R<sub>4</sub>, R<sub>8</sub>, R<sub>9</sub>, R<sub>10</sub>, R<sub>11</sub>, R<sub>12</sub>, R<sub>13</sub>, R<sub>14</sub>, R<sub>15</sub>, R<sub>16</sub>, R<sub>17</sub>, R<sub>18</sub>, and R<sub>19</sub> are selected from saturated and unsaturated hydrocarbons containing from 1 to 7 carbon atoms per molecule, and hydrogen; and

wherein said anion is selected from the group consisting of halides of: Group IIIA metals, copper, zinc, iron and phosphorus.

- 19. A process in accordance with claim 18 wherein said anion is selected from the groups consisting of AlCl<sub>4</sub>, Al<sub>2</sub>Cl<sub>7</sub>, Al<sub>3</sub>Cl<sub>10</sub>, GaCl<sub>4</sub>, Ga<sub>2</sub>Cl<sub>7</sub>, Ga<sub>3</sub>Cl<sub>10</sub>, CuCl<sub>2</sub>, Cu<sub>2</sub>Cl<sub>3</sub>, Cu<sub>3</sub>Cl<sub>4</sub>, ZnCl<sub>3</sub>, FeCl<sub>3</sub>, FeCl<sub>4</sub>, Fe<sub>3</sub>Cl<sub>7</sub>, PF<sub>6</sub>, and BF<sub>4</sub>.
- 20. A process in accordance with claim 18 wherein said ionic liquid has the formula  $R_1R_2R_3NH^+Al_2Cl_7$ .
- 21. A process in accordance with claim 18 wherein said ionic liquid has the formula (CH<sub>3</sub>)<sub>3</sub>NH<sup>+</sup>Al<sub>2</sub>Cl<sub>7</sub>.
- 22. A process in accordance with claim 12 wherein said hydrocarbon feed stream comprises at least 50 weight-% isopentane, based on the total weight of said hydrocarbon feed stream.
- 23. A process in accordance with claim 12 wherein said hydrocarbon feed stream comprises in the range of from about 50 to about 95 weight-% isopentane, based on the total weight of said hydrocarbon feed stream.

- 24. A process in accordance with claim 12 wherein said hydrocarbon feed stream comprises in the range of from about 80 to about 98.5 weight-% isopentane, based on the total weight of said hydrocarbon feed stream.
- 25. A process in accordance with claim 12 wherein said conversion conditions include a temperature in the range of from about 100°F to about 1000°F.
- 26. A process in accordance with claim 12 wherein said conversion conditions include a temperature in the range of from about 140°F to about 250°F.
- 27. A process in accordance with claim 12 wherein said conversion conditions include a temperature in the range of from about 150°F to about 220°F.
- 28. A process in accordance with claim 12 wherein said  $C_4$  paraffin of said product stream is isobutane and said  $C_6$  paraffin of said product stream is a hexane isomer.
- 29. A process in accordance with claim 12 wherein said initiator is selected from the group consisting of: 1) an olefin having in the range of from 2 to 20 carbon atoms per molecule, 2) an alkyl halide wherein said alkyl halide has in the range of from 2 to 20 carbon atoms per molecule, and combinations thereof.